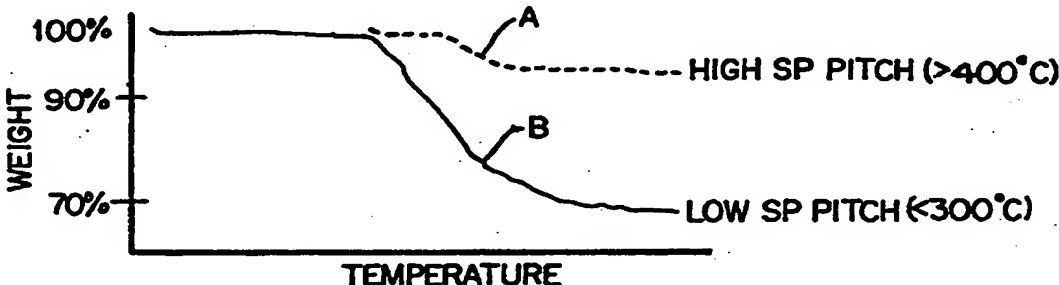


PCTWORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau

INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶ : C10C 3/00, C04B 35/52, 38/00	A1	(11) International Publication Number: WO 99/61549 (43) International Publication Date: 2 December 1999 (02.12.99)
(21) International Application Number: PCT/US99/11279 (22) International Filing Date: 21 May 1999 (21.05.99) (30) Priority Data: 60/086,371 22 May 1998 (22.05.98) US 09/112,994 10 July 1998 (10.07.98) US (71) Applicant: ALLIEDSIGNAL INC. [US/US]; 101 Columbia Road, P.O. Box 2245, Morristown, NJ 07962-2245 (US). (72) Inventors: MURDIE, Neil; Apartment D, 1621 N. Riverside Drive, South Bend, IN 46616 (US). PIGFORD, James; 1005 Royal Vineyard, South Bend, IN 46637 (US). WOOD, Mike; 1921 Cross Creek Drive, South Bend, IN 46628 (US). DILLON, Frank; 51732 James Lawrence Parkway, Granger, IN 46530 (US). PARKER, Charles; 52199 Arrowhead Circle, Granger, IN 46530 (US). HEMSTAD, Stan; 50634 Stonington Drive, Granger, IN 46530 (US). (74) Agents: CRISS, Roger, H. et al.; AlliedSignal Inc., Law Dept., (Amy Olinger), 101 Columbia Road, P.O. Box 2245, Morristown, NJ 07962-2245 (US).		(81) Designated States: AU, CA, CN, CZ, IN, JP, KR, PL, RU, European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE). Published <i>With international search report. Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>
(54) Title: METHODS FOR MAKING A PITCH-BASED CARBON FOAM  <p>(57) Abstract A mesophase pitch material having a melting point in excess of 350 °C has a solvent added thereto to provide a solvated mesophase pitch. A low molecular weight solvent is used so that the melting point can be brought low enough to create a carbon foam at a convenient temperature. The solvent is then removed by heat and/or vacuum and, consequently, the pitch reverts to a high melting point of approximately greater than 350 °C. The pitch can then be heated or carbonized without an oxidative stabilization step. Alternatively, a solvated mesophase pitch material may be used initially for foaming.</p>		

BEST AVAILABLE COPY

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AL	Albania	ES	Spain	LS	Lesotho	SI	Slovenia
AM	Armenia	FI	Finland	LT	Lithuania	SK	Slovakia
AT	Austria	FR	France	LU	Luxembourg	SN	Senegal
AU	Australia	GA	Gabon	LV	Latvia	SZ	Swaziland
AZ	Azerbaijan	GB	United Kingdom	MC	Monaco	TD	Chad
BA	Bosnia and Herzegovina	GE	Georgia	MD	Republic of Moldova	TG	Togo
BB	Barbados	GH	Ghana	MG	Madagascar	TJ	Tajikistan
BE	Belgium	GN	Guinea	MK	The former Yugoslav Republic of Macedonia	TM	Turkmenistan
BF	Burkina Faso	GR	Greece	ML	Mali	TR	Turkey
BG	Bulgaria	HU	Hungary	MN	Mongolia	TT	Trinidad and Tobago
BJ	Benin	IE	Ireland	MR	Mauritania	UA	Ukraine
BR	Brazil	IL	Israel	MW	Malawi	UG	Uganda
BY	Belarus	IS	Iceland	MX	Mexico	US	United States of America
CA	Canada	IT	Italy	NE	Niger	UZ	Uzbekistan
CF	Central African Republic	JP	Japan	NL	Netherlands	VN	Viet Nam
CG	Congo	KE	Kenya	NO	Norway	YU	Yugoslavia
CH	Switzerland	KG	Kyrgyzstan	NZ	New Zealand	ZW	Zimbabwe
CI	Côte d'Ivoire	KP	Democratic People's Republic of Korea	PL	Poland		
CM	Cameroon	KR	Republic of Korea	PT	Portugal		
CN	China	KZ	Kazakhstan	RO	Romania		
CU	Cuba	LC	Saint Lucia	RU	Russian Federation		
CZ	Czech Republic	LI	Liechtenstein	SD	Sudan		
DE	Germany	LK	Sri Lanka	SE	Sweden		
DK	Denmark	LR	Liberia	SG	Singapore		
EE	Estonia						

METHODS FOR MAKING A PITCH-BASED CARBON FOAM

This patent application claims priority upon U.S. provisional patent application 60/086,371, filed May 22, 1998.

This is a continuation-in-part of U.S. Patent Application Serial No. 08/970,558, filed November 14, 1997.

The present invention relates generally to the utilization of a solvated mesophase pitch to make a carbon foam, and in particular to the use of a solvated mesophase pitch to make a carbon foam which requires little or no oxidative stabilization prior to carbonization of the carbon foam.

Carbon-carbon composites are widely used for aircraft brake friction materials. Although carbon-carbon is attractive because it is lightweight and can operate at very high temperatures, the use of carbon-carbon raw material entails the use of an expensive material. Expensive carbon fiber is a significant component; sometimes up to 45 percent fiber is used in making the composite. Additionally, the manufacture of carbon-carbon is a time-consuming process. Long cycle times are undesirable in a modern manufacturing environment. Copending U.S. Patent Application Serial No. 08/970,558 describes inventions for making an aircraft brake friction material by means of a carbon-carbon composite material made from densified carbon foam. Copending U.S. Patent Application Serial No. 08/970,558 is incorporated by reference in its entirety herein. The manufacturing process disclosed therein may be generally described by the steps of utilizing a precursor material (thermoset or thermoplastic), foaming the precursor material, oxygen stabilization for foams produced from thermoplastics, carbonization, optional heat treatment, densification, and a subsequent heat treatment. As disclosed in USSN 08/970,558, when a foam is made from a thermoplastic such as a mesophase pitch, it may be necessary to cross link the foam by oxidation before it can be heated to carbonization temperatures. Without this oxidation (stabilization) step, the pitch may melt when it is heated. The oxidative stabilization step can be a time-consuming process (up to 100 hours). The objective of the inventions disclosed herein is to reduce the time required for processing the carbon foam by eliminating or replacing, or shortening, the oxidative stabilization step.

The inventions disclosed herein utilize solvated mesophase pitches which offer the potential for foaming at low temperatures, followed by carbonization at high temperatures without the need for stabilization. By using a solvated mesophase pitch, a carbon foam preform can be produced
5 by the methods described in copending USSN 08/970,558 and herein. Removal of the "solvent" fraction of the mesophase ensures that the mesophase pitch has a higher softening point (greater than 350°C) than the onset temperature of carbonization (300-500°C). Thus, the mesophase carbonizes before it can soften, thereby eliminating the requirement for
10 stabilization.

The present invention obviates the need for oxidative stabilization and provides solutions to the above by providing a pitch-based carbon foam suitable for carbonization, comprising a solidified open-cellular carbon foam having a softening point to greater than 350°C, the foam made from a
15 solvated pitch material having a softening point below 300°C which was heated to effect melting of the pitch material, foamed to provide the open-cellular carbon foam and the solvent removed to raise the softening point to greater than 350°C and solidify the foam, to provide the pitch-based carbon foam suitable for carbonization.

20 Figure 1 is a graph illustrating the weight losses of high and low softening point pitches during carbonization;

Figure 2 is a graph illustrating the increase of the softening point of the carbon foam during carbonization.

25 Figure 3 illustrates the advantages of utilizing a solvated mesophase pitch A, as compared to utilizing a conventional pitch B.

The inventions disclosed herein utilize a solvated mesophase pitch to solve the problem of eliminating or replacing, or shortening, the oxidative stabilization step. The natural, unsolvated melting point of the pitch is generally in excess of 350°C, such that the pitch will begin to carbonize
30 before it begins to melt. Using a low molecular weight solvent, the melting point can be lowered low enough to be foamed at a convenient temperature, then the solvent is removed by heat with or without vacuum. Consequently, the pitch reverts to its high melting point and may be carbonized without a

stabilization step. The advantages of this approach can be realized if the devolatilization or solvent removal step is faster than the oxidation step it eliminates.

The process may be generally described by the following steps:

- 5 • Plasticization: A high softening point mesophase pitch (greater than 350°C) is plasticized with solvent to a lower softening point below 300°C.
- Heating: Heating solvated mesophase pitch to melt at one atmosphere, such as heating in an autoclave or other device such that
10 the pitch can be pressurized with nitrogen gas.
- Foaming: Cause material to foam by either vaporization of volatile material or a pressure drop, to provide an open cellular structure.
- Solvent removal: Vaporization or vacuum draws out plasticizer causing
15 the softening point of the pitch foam to rise, and solvent extraction continued until the softening point increases to greater than 350°C.
- Carbonization: The foam can now be carbonized (heating to the range of 600-2000°C) and oxidative stabilization is not required because the
 pitch will carbonize without melting.

20 The process generally described above has an additional advantage over creating a carbon foam from a low softening point pitch with a physical blowing agent, in that the weight loss upon carbonization will be less for the high softening point pitch. This is illustrated in Figure 1 which demonstrates that as temperatures increase during carbonization, the high softening point
25 pitch experiences considerably less weight loss. Additionally, the high softening point pitch will have higher viscosity which will provide more alignment of mesophase within the strut regions of the foam. Also the lower weight loss of the high softening point pitch in curve A will provide less cracking during carbonization.

Pitches:

30 In general, the following pitches may be utilized for the process and materials disclosed herein:

1. Mesophase pitches
2. Isotropic (coal tar, petroleum derived)

- a. Isotropic (coal tar and petroleum derived pitches) may be converted to mesophase by a thermal treatment and subsequent extraction; or
- b. They can also be converted to mesophase by use of a catalyst and extraction, leading to a pitch with softening point greater than 350°C

3. Synthetic mesophase pitches can also be used, eg, derived from naphthalene/anthracene or alkyl benzene.
 - a. The above pitches have a low softening point of approximately 200 to 300°C. They can be treated as follows: devolatilization with vacuum, or treat with heat and then extract the mesophase to increase the softening point to 350°C, then add back the plasticizer to obtain the desired softening point.

Another way to treat mesophase pitches derived from isotropic, synthetic or low softening point pitches is to partially, oxidatively, stabilize or thermoset the pitch to increase the softening point to greater than 350°C then add back plasticizer and reduce the softening point below 300°C. The general approach is to provide a mesophase pitch with softening point of greater than 350°C and add back a solvent/plasticizer to reduce softening point to less than 300°C. Solvated mesophase pitches have been provided by and disclosed in Kalback, et al., U.S. Patent 5,259,947, issued November 9, 1993 to Conoco Inc.

Plasticizers:

The functions of plasticizers is to lower the softening point of mesophase pitch without modification of the mesophase characteristics and to be subsequently easily removable by vacuum or heat to provide an ephemeral solvent. Examples of plasticizers comprise tetrahydrofuran, toluene, pyridine, benzene, xylene, which is not an exhaustive list. These are aromatic or conjugated compounds which are hydrogen donors. They will interact with and solubilize the mesophase pitch polyaromatic molecules.

Foaming:

Several approaches can be utilized to foam the above described solvent-pitch mixtures. The process may be generally described by using the solvent as a native blowing agent, and then:

- a. Heat the mixture to a temperature T_0 , where
- 5 b. The mixture becomes soft
- c. Pressurize the mixture to P_0
- d. Lower the pressure to P_1 where the solvent/plasticizer foams bubbles; it is desirable to nucleate many small bubbles simultaneously
- 10 e. Lower the pressure further to open the bubbles to the outside (make open cells)
- f. Then continue to extract solvent to cause solidification and/or raise the melting point of the foam.

Several variations may be utilized within this process. First, another
15 physical blowing agent can be added, such as N_2 , CO_2 , chlorofluorocarbons, air, hydrofluorocarbons, water vapor, paraffin (eg. pentane) and perform cycles 1a-1e above. Second, add a chemical blowing agent (e.g. azides or carbonates) which liberate N_2 or CO_2 on heating. Perform cycles 1a-1e above. Note that in the case of using a chemical blowing agent, and some
20 physical blowing agents which have boiling points above room temperature, that performing cycles 1a-1e will work with $P_1 = P_0$. Third, add physical blowing agents such as N_2 and CO_2 or paraffin by heating under pressure of the gas and cool under pressure. This physical blowing agent plus the plasticizer can subsequently both be used to foam the pitch following cycles
25 1a-1e above. Fourth, perform the whole process (steps 1a-1e above) at one pressure, e.g. 1 atmosphere. When a physical blowing agent such as N_2 , CO_2 or paraffin is used, these may plasticize the pitch as well, so that when they come out of solution on foaming the pitch solidifies, retaining the other plasticizer, e.g. pyridine, tetrahydrofuran, benzene, and so on, which would
30 have to be removed by vacuum. This allows flexibility and high precision control of pore size distribution which is subsequently important, if not critical, for subsequent densification, if required. The control of pore size distribution leads to the control of the density and microstructure, and hence the

mechanical properties of the foam. The benefit pertaining to viscosity is that by foaming at a higher viscosity, the alignment of mesophase in the strut regions of the foam will be enhanced, providing improved orientation in struts and better thermal and mechanical properties. There is a well-defined viscosity range which allows foaming of mesophase pitches to occur. It is essential that foaming be performed at the higher end of the viscosity range to attain optimum shear and alignment. The process described above yields a carbon foam which requires little or no oxidative stabilization since the softening point of the pitch after extraction of plasticizers is greater than the carbonization onset temperature, and thus melting or bloating will not occur. In other words, as the pitch is heated, the melting point will continue to increase by removal of hydrogen and condensation of molecules, such that the melting point is always higher than the temperature at which the condensation is occurring. Figure 2 illustrates this relationship wherein as temperature is increased over time during carbonization, the softening point also increases and remains above the temperature of carbonization.

Carbonization:

Generally, carbonization is performed to temperatures between 600°C to 2000°C. As illustrated in Figure 3, the use of a solvated mesophase pitch material provides a higher carbon yield, and a slower rate of devolatilization during carbonization. Therefore, there is a reduction in damage to the foam (cracks and so on) both in bulk foam and microcracks within the struts. Further, slow devolatilization retains the molecular alignment in the struts better than would a rapid devolatilization during carbonization. In Figure 3, curve A represents the utilization of a solvated mesophase pitch as described herein, while curve B illustrates the utilization of a conventional mesophase pitch such as Mitsubishi AR pitch.

Example:

A Conoco solvated mesophase pitch, made in accordance with Kalback, et al. U.S. Patent No. 5,259,947, was used to create a foam in an autoclave. 25g of the Conoco solvated pitch was heated in an aluminum sample boat in a flow of dry nitrogen gas within an autoclave vessel. The temperature/pressure/time cycle used was as follows: (1) pitch heated from

25°C to 340°C at (system open, nitrogen purge) 160°C /hr, (2) sample soak at 340°C for 20 minutes (system open, nitrogen purge), (3) autoclave system closed and sample/vessel pressurized with 1000 psi nitrogen gas, (4) sample cooled from 340°C to 266°C at 80°C /hr, (5) sample heated from 266°C to 290°C at 80°C /hr, (6) sample soaked at 290°C for two hours, (7) vessel/sample depressurized from 1000 psi to 15 psi in three seconds, (8) sample allowed to cool from 290°C to 25°C at 25°C/hr. The foam was placed in the vacuum oven overnight at 90°C. The foam was carbonized without an intermediate oxidative stabilization step. The carbonization cycle involved heating the part to 810°C in thirty-three hours, then holding for one hour. The carbon yield (ie., weight residue remaining after carbonization) was 81.2 weight %. The carbonization was successful without bloating or melting of the foam.

We believe that a preferred method for carrying out the invention is to provide a solvated mesophase pitch (made in accordance with Kalback, et al. U.S. Patent No. 5,259,947) that is heated from 25°C to 300°C in two hours under flowing nitrogen gas in an open autoclave system. When 300°C is attained, the vessel (sample) is pressurized to 800 psi. The vessel is allowed to cool down to a temperature of 268°C. This temperature is maintained for a 2.5 hour soak, after which the vessel is depressurized from 800 psi to 15 psi within two-three seconds. The resultant foam within the vessel is allowed to cool slowly such that it takes 8-10 hours to cool from 268°C to 25°C. Experiments performed indicate that the microstructure and physical properties of these foams are profoundly influenced by the temperatures/pressures used in the process. Small pore sizes are favored by lower operating temperatures and pressures.

The inventions disclosed herein illustrate that a carbon foam material can be provided either without the need for an oxidative stabilization of the material or with the oxidative stabilization, disclosed in copending USSN 08/970,558, shortened significantly and preferably eliminated.

We claim:

1. A method for making a pitch-based carbon foam, comprising the steps of providing a solvated pitch material having a softening point of below 300°C, heating the solvated pitch material to effect melting thereof, foaming the material to provide an open-cellular carbon foam, removing the solvent from the carbon foam and raising the softening point to greater than 350°C such that the carbon foam solidifies, and heating the foam within the range of 600-2000°C to remove volatiles therefrom and provide the pitch-based carbon foam.
2. The method in accordance with Claim 1, wherein the pitch material comprises one of a mesophase pitch, suitably modified isotropic pitches, coal tars, petroleum derived pitches, and synthetic pitches .
3. The method in accordance with Claim 1, wherein the solvent of the pitch material comprises one of tetrahydrofuran, toluene, pyridine, benzene, and xylene.
4. The method in accordance with Claim 1, wherein the foaming step comprises the use of a physical blowing agent comprising one of N₂, CO₂, chlorofluorocarbons, air, hydrofluorocarbons, water vapor, pentane.
5. The method in accordance with Claim 4, wherein the final heating step comprises carbonization wherein as volatiles are removed the softening point of the carbon foam also increases.
6. The method in accordance with Claim 1, wherein the foaming step is accomplished by one of (a) continued heating and (b) continued heating and lowering the pressure.
7. A pitch-based carbon foam suitable for carbonization, comprising a solidified open-cellular carbon foam having a softening point to greater than 350°C, the foam made from a solvated pitch material having a softening point below 300°C which was heated to effect melting of the pitch material, foamed to provide the open-cellular carbon foam and the solvent removed to raise the softening point to greater than 350°C and solidify the foam, to provide the pitch-based carbon foam suitable for carbonization.

8. The pitch-based carbon foam in accordance with Claim 7, wherein the foam is heated within the range of 600-2000°C to remove volatiles therefrom and provide a carbonized pitch-based carbon foam.

9. The pitch-based carbon foam in accordance with Claim 7, wherein the pitch material comprised one of a mesophase pitch, suitably modified isotropic pitches, coal tars, petroleum derived pitches, and synthetic pitches.

10. The pitch-based carbon foam in accordance with Claim 7, wherein the solvent of the pitch material comprises one of tetrahydrofuran, toluene, pyridine, benzene, and xylene.

11. The pitch-based carbon foam in accordance with Claim 7, wherein foaming was accomplished by using a physical blowing agent comprising one of N₂, CO₂, chlorofluorocarbons, air, hydrofluorocarbons, water vapor, pentane.

12. The pitch-based carbon foam in accordance with Claim 7, wherein the solvated pitch material was provided by adding a solvent to a pitch material having a softening point of greater than 350°C in order to lower the softening point to below 300°C.

13. A method for making a pitch-based carbon foam, comprising the steps of providing a pitch material having a softening point of greater than 350°C, adding a solvent to the pitch material which lowers the softening point of the material to below 300°C, heating the solvated pitch material to effect melting thereof, foaming the material to provide an open cellular carbon foam, removing the solvent from the carbon foam and raising the softening point to greater than 350°C such that the carbon foam solidifies, and heating the foam within the range of 600-2000°C to remove volatiles therefrom and provide the pitch-based carbon foam.

14. The method in accordance with Claim 13, wherein the pitch material comprises one of a mesophase pitch, suitably modified isotropic pitches, coal tars, petroleum derived pitches, and synthetic pitches.

15. The method in accordance with Claim 13, wherein the solvent comprises one of tetrahydrofuran, toluene, pyridine, benzene, and xylene.

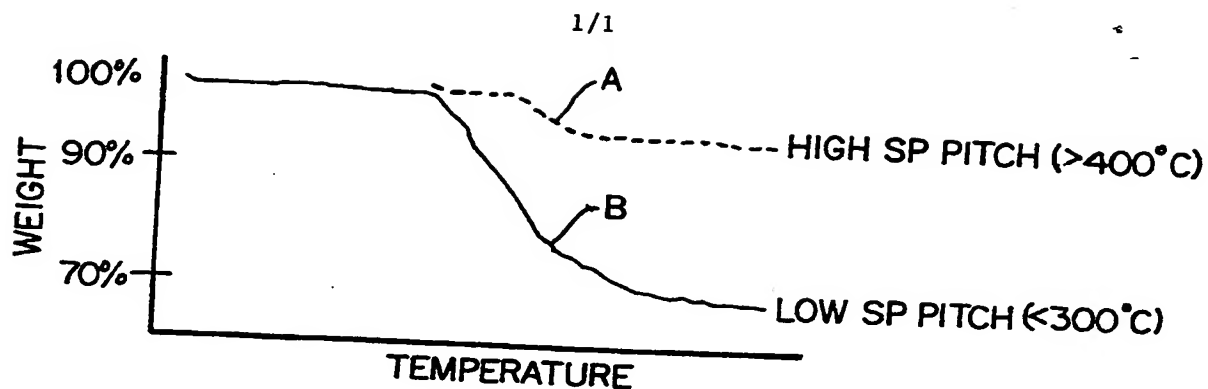


FIG. 1

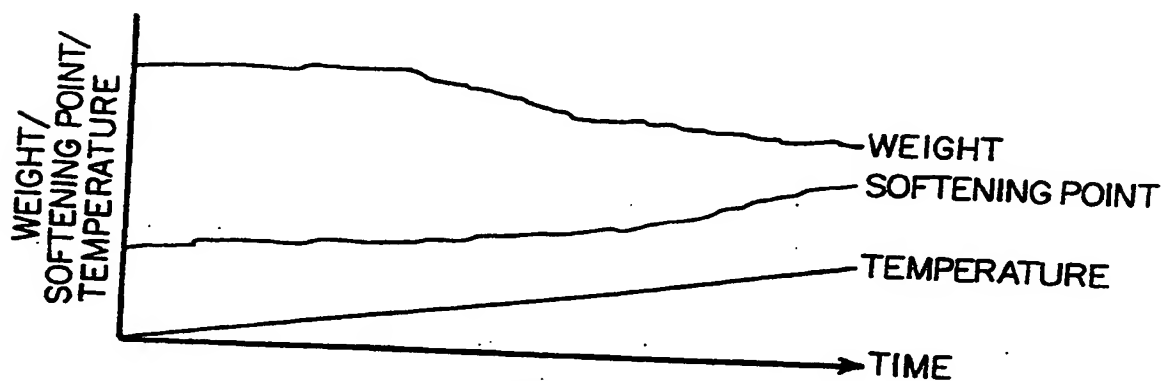


FIG. 2

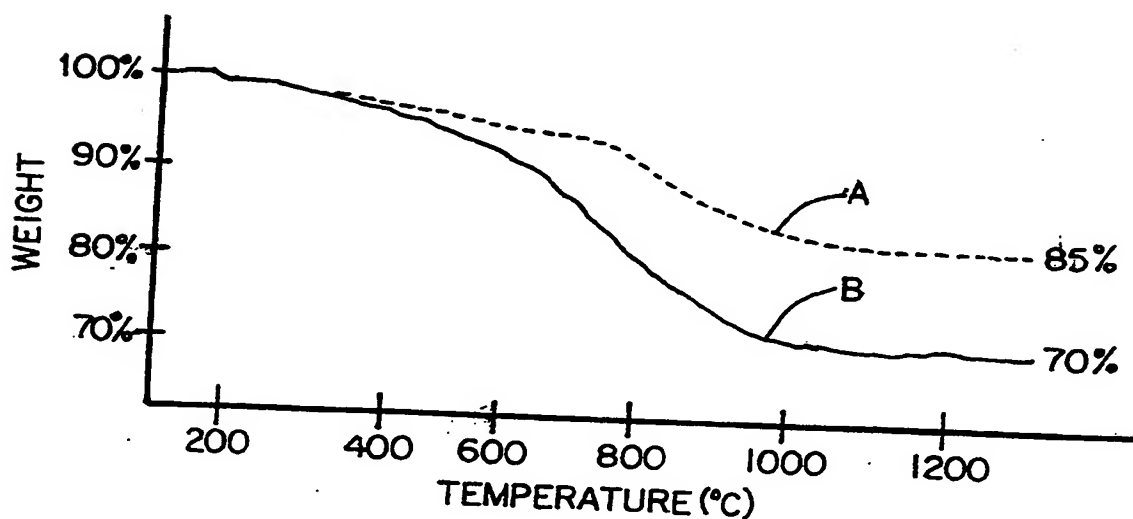


FIG. 3

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 99/11279

A. CLASSIFICATION OF SUBJECT MATTER
IPC 6 C10C3/00 C04B35/52 C04B38/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 C10C C04B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	WO 93 24590 A (CONOCO CORP.) 9 December 1993 (1993-12-09) page 4, line 29 - page 5, line 5 page 5, line 22 - line 32 page 6, line 25 - page 7, line 19 page 8, line 16 - line 19; claims 1,3,5,17; example 1 ---	1-15
Y	DATABASE WPI Week 9028 Derwent Publications Ltd., London, GB; AN 90-213280 XP002900628 & JP 02 142891 A (KAWASAKI STEEL CORP.), 31 May 1990 (1990-05-31) abstract -----	1-15

☐ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

* Special categories of cited documents:

- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier document but published on or after the international filing date
- "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the international filing date but later than the priority date claimed

- "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
- "S" document member of the same patent family

Date of the actual completion of the international search

24 September 1999

Date of mailing of the international search report

28. 10. 99

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
Fax: (+31-70) 340-3016

Authorized officer

Ulrika Nilsson

BEST AVAILABLE COPY

INTERNATIONAL SEARCH REPORT
Information on patent family members

International application No.
PCT/US 99/11279

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO 9324590 A1	09/12/93	AU 662644 B	07/09/95
		AU 4389893 A	30/12/93
		CA 2135933 A	09/12/93
		CN 1034221 B	12/03/97
		CN 1083511 A	09/03/94
		CN 1139145 A	01/01/97
		DE 69308134 D,T	07/08/97
		EP 0643755 A,B	22/03/95
		JP 7507351 T	10/08/95
		NO 944653 A	02/12/94
		NZ 247709 A	24/02/95
		US 5540832 A	30/07/96
		US 5540903 A	30/07/96

BEST AVAILABLE COPY